HYDRODYNAMIC AND THERMAL PERFORMANCE OF TWISTED TAPE INSERT PROVIDED IN HEAT EXCHANGER TUBES: A REVIEW

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**ABSTRACT**

This work presents a review of the research recent results concerning the augmentation of hydrodynamic and thermal performance of various twisted tape inserts in heat exchanger tubes. The thermal and hydrodynamic correlations for various twisted tape elements have been summarized. A comparative study of thermal and hydrodynamic performance of numerous twisted elements has also been reported to understand the result of applications of twisted tape inserts in heat exchanger tubes. The literature review found that multiple twisted tapes heat exchanger tube shape enhanced hydrodynamic and thermal performance than other comparable twisted tape inserts heat exchanger tube shapes. The review of twisted tape inserts techniques existing in this paper will be helpful to the investigators working in this field.

**Keywords:** Heat transfer; heat exchangers; passive techniques; fluid flow.

1. INTRODUCTION

Energy is a primary need to live our daily life at expenses of some valuable things such as environment degradation by using fossil fuels. Heat exchangers play a heating/cooling role in various fields like electric power, metallurgy, chemical engineering, refrigeration, and air-conditioning etc. by Sunil et al. (2019), Singh Suri et al. (2017) and Kumar & Kim (2016). Circular tubes are widely used in heat exchange equipment's because of the ease of production and its capability of withstanding a high pressure Kumar et al. (2017) and Singh et al. (2018). Insertion of twisted tapes into a tube provides a simple passive technique for enhancing the heat transfer by introducing vortex generator into the bulk flow by breaking laminar sub layer at the tube wall due to repeated changes in the surface geometry. While insert technology is employed for augmented heat transfer, pressure drop would be improved by inserting twisted tape in a tube Kumar et al. (2017), Singh et al. (2018), Yashwant Singh et al. (2018) and Maithani et al. (2019).

Twisted tapes with various shapes were proposed and utilized by various researchers. Numerous investigations have carried out the investigators in twisted tape inserts and thus, there is need to review the past and current research so that the further research scopes can be identified and implemented. The present article is thus aimed with following objectives:

- To review the augmentation in heat transfer and pressure drop in heat exchanger tubes equipped with various twisted tape inserts.
- To arrange the heat transfer and pressure drop correlations of a variety of twisted tape inserts in heat exchanger tubes.
- To carry out comparative study of heat transfer and pressure drop of heat exchanger tubes equipped with twisted tape insert.

In order to achieve the desired objectives, the article is structured batch wise for each objective clearly addressed and explained in their respective context.

2. LITERATURE REVIEW ON TWISTED TAPE INSERT IN HEAT EXCHANGER TUBES

Efforts for improving the thermal and hydrodynamic performance of heat exchangers have directed the investigation in the direction of disturbing the viscous sub layer by proving twisted tape inserts. Many investigations have been carried out to analysis the flow field characteristics of thermal and hydrodynamic of twisted tape insert tubes. Singh et al. (2017) examined the efficiency factor of twisted tape round tube for stable heat flux. The Reynolds number covered in the range of 6300 to 22500 for co-twist arrangements in the turbulent flow of air in the round tube. Kongkaitpaiboon et al. (2010) experimentally investigated the augmentation of thermal hydrodynamic performance in circular tube equipped with perforated conical rings. It was concluded that the augmentation in thermal and hydraulic performance achieved was 3.67 and 2.89 times more than plain circular tube, respectively. Li and Guo (2009) carried out experimental and numerical investigation of turbulent heat transfer and stream resistance in an improved round tube equipped with twisted tape inserts.

Promvonge (2008) experimentally studied the thermal and hydrodynamic performance of circular HET fitted with wire coiled inserts. The maximum value of thermal and hydrodynamic performance has been found to be 2.13 within the range of the parameters examined. Zhang and Zhang and Liu (2013) carried out numerical analysis of 3D turbulence fluid flow to study heat transfer and fluid flow.
characteristics for helical screw tape inserts without core rod inserts. Shabanian et al. (2011) performed an experimental and computational analysis to study the thermal performance in an air cooled round tube fitted with three different types of tape inserts. Krishna et al. (2009) investigate thermal performance enhancement technique and concluded that heat transfer and friction factor enhancement in helical and left–right twisted tape collectors was better than the plain circular tube collector and it was 3.78 and 1.45 times more than that of plain tube collector. Eiamsa-ard et al. (2006) carried out a comparative experimental study on thermal performance in a round tube with regularly spaced tape inserts and plane tube. The results of the study reveal that thermal performance increases with decrease of space ratio.

Naphon et al. (2006) carried out an experimental study to the behaviour of heat transfer and flow friction in horizontal double circular tubes equipped with tape inserts having length and thickness 2.0 mm and 0.01 mm respectively. Maddah et al. (2014) conducted an experimental investigation on heat transfer augmentation of Alumina/water nanofluid in a flat double circular tube with customized tape inserts. Sharma et al. (2009) experimentally examined the thermal performance by establishing mathematical relationship among Nusselt number and friction factor. The working Alumina/water nanofluid was circulated through a circular round tube of with tape inserts. Eiamsa-ard et al. (2012) carried out an experimental investigation to study thermal performance using helically inserts by using three different \( \gamma_h \) and helical \( H_h \) 2.0-3.0. It was found that by inserting helical tape inserts the value of hydrodynamic and thermal performance was significantly higher than conventional helical tape. Eiamsa-ard and Wongcharee (2013) examined the thermal performance in circular tube fitted with dual tape inserts in three different types of geometrical configurations. Jaisankar et al. (2009) experimentally investigated the efficiency factor of twisted inserts with various spacer length inserts in a thermosyphon solar water heating system.


Sarada et al. (2010) studied the \( \text{Nu}_{th} \) increase in a round tube with changing breadth of tape inserts. Their outcome demonstrates that the utmost augmentation in thermal and hydraulic performance is observed to be 2.16 and 2.66 times of that of the plain round tube, respectively. Eiamsa-ard and Promvonge (2010) experimentally studied thermal behaviour of plane circular pipe equipped with multi tape inserts along with various clock wise and counter clockwise tape inserts. Eiamsa-ard et al. (2006) experimentally studied the behaviour of flow friction and heat transfer in two-fold round tube fitted with tape inserts. A significant improvement were noticed in both flow friction and heat transfer. Eiamsa-ard et al. (2010) examined thermal performance in a round tube fitted with pooled devices among the tape inserts and steady or at regular intervals varying wire coil insert. Eiamsa-ard et al. (2010) experimentally investigated the efficiency factor in a circular pipe fitted with delta-winglet tape inserts. Sharma et al. (2003) explored a new method to enhance heat transfer in a round pipe equipped with twisted tape inserts. Sharma et al. (2005) discovered new mathematical generalized correlations for heat transfer and fluid flow for a round pipe fitted with twisted tape inserts. Yilmaz et al. (2003) carried out an experimental investigation to study the effects of special geometry of various components on efficiency factor. Chang et al. (2007) conducted an experimental investigation on twisted tape with cut and explored enhancement in performance of twisted tape with cut in comparison to smooth round tube. Chang et al. (2007) carried out an experimental investigation to study thermal performance in a round tube fitted with jagged tape inserts.

Seemawute and Eiasma-ard (2010) experimentally investigated the thermal performance through a round pipe having peripherally-cut twisted tape inserts. The thermal performance in round tube with peripherally-cut tape inserts with alternate axis, peripherally-cut tape inserts and multi tape inserts was found 23%, 45% and 62%, respectively than that of plain round tube. Eiamsa-ard et al. (2010) experimentally examined the behaviour of thermal performance for a round tube fitted with sole tape inserts, complete length dual tape inserts and on a regular basis spaced dual tape inserts below identical wall heat flux circumstances. Bhiyya et al. (2013) experimentally examined the thermal performance for a turbulent flow through a round tube fitted with perforated tape inserts. The experimental consequences revealed a significant augmentation in thermal performance than the consequences of plain round tube. Karami et al. (2012) experimentally analysed the thermal performance in an air cooled round tube heat exchanger equipped with typical tape inserts. Murugesan et al. (2011) experimentally examined the efficiency factor for plain round pipe fitted with V-cut tape insert.

Murugesan et al. (2010) experimentally investigated the thermal performance of a double round tube fitted with simple plane tape inserts and tape having wire nails. Murugesan et al. (2010b) experimentally investigated the efficiency factor for a double circular tube having square-cut tape inserts and plain tape inserts. Their results revealed that the thermal performance for round tube equipped with square-cut tape inserts were significantly more than plain tape inserts. Promvonge and Eiasma-ard (2007) experimentally studied the augmentation in thermal hydrodynamic performance of round tube attached with narrow conical ring. Nagarajan et al. (2010) experimentally examined the augmentation of thermal hydrodynamic performance of round tube attached with left-right tape inserts. New empirical correlations based on experimental data were introduced for thermal performance.

Thianpong et al. (2009) carried out an investigation to examine the thermal performance in a dimpled shape circular tube fitted with different tape inserts. Sivashanmugam and Suresh (2006) analysed the circular pipe fitted with helical twisted tape inserts experimentally. Sivashanmugam and Suresh (2007) experimentally determined the efficiency factor for circular pipe incorporated with various helical ST inserts having spacer distance end to end 100 mm, 200 mm, 300 mm and 400 mm. Chang et al. (2009) experimentally examined the thermal performance in a round tube equipped with various tape inserts. Eiamsa-ard et al. (2009) experimentally examined the thermal performance in turbulent section for round tube fitted through small length tape inserts. Promvonge (2008) experimentally examined the thermal performance in turbulent flow within a round pipe fitted with wire coils shape inserts and tape inserts.

Bharadwaj et al. (2009) analysed the augmentation of thermal hydrodynamic performance of round tube attached with grooved twisted tapes. Mazumder and Saha (2008) experimentally investigated the thermal performance in heat exchanger fixed with tape inserts for turbulent flow. Murugesan et al. (2012) carried out an experimental investigation of thermal performance through circular tube incorporated with various twisted tape inserts. The range of Reynolds number (Re) was varied from 2000 to 12000 and water was taken as base fluid in the experiment. Wongcharee and Eiamsa-ard (2011) experimentally determined the thermal performance of round tube attached with customized tape inserts with alternating alignment. Zhang et al. (2012) experimentally examined the thermal performance in a round pipe with three and four tape inserts. Their analysis shows a significant improvement of thermal performance for three and four tape inserts. Ray and Date (2001) investigated thermal performance in heat exchanger fitted with tape inserts. The outcome of the analysis yields a significant improvement in thermal performance for twisted tape inserts.
as compared plain heat exchanger. Salam et al. (2013) conducted an experimental analysis to study the behaviour of flow friction and heat transfer in turbulent flow in a heat exchanger with rectangular slug tape inserts. Pal and Saha (2014) experimentally investigated the efficiency factor in a tube fitted with coiled corrugation roughness along with oblique teeth tape inserts. The working fluid in the experiment was taken viscous oil with laminar flow. Klaczak (2000) investigated the efficiency factor in round tube with erect copper pipe tape inserts. Experiments were carried out with air as working fluid and four tape inserts of twist ratio ranging from 1.63 to 5.28 and the range of Reynolds number varied from 110 to 1500. Rout and Saha (2013) examined the behaviour of heat transfer and pressure for laminar flow inside a round pipe with tape inserts constituted from wire coil helical screw.

Agarwal and Rao (1996) experimentally studied the augmentation of thermal hydrodynamic performance of double pipe with wire coiled inserts. The experiments examined double pipe in succession by keeping wall temperature constant. Sivashannugam and Suresh (2006) experimentally examined the behaviour of heat transfer and pressure drop in laminar stream in circular pipe with twisted tape as inserts for twist ratio values of 1.94, 2.92, 3.92, and 4.88. Wongscharee and Eiamsa-ard (2011) experimentally examined the thermal performance in round tube along with alternating anti-clockwise and clockwise tape inserts. It was found that the performance of round tube alternating anti-clockwise and clockwise tape inserts significantly enhances the thermal performance as compared to tube with tape inserts. Sujoy et al. (2012) experimentally examined efficiency factor for laminar flow in round tube made up of circular passage with centre-cleared.


Pramanik and Saha (2006) experimentally examined the thermal performance in laminar stream flowing in round tube fitted with flat rectangular and square passage fitted tape inserts. Their investigation showed that the performance of twisted tape having regularly spaced geometry was improved than that full-length twisted tape inserts. Bilen et al. (2001) examined the heat transfer rate of heat exchanger tube equipped with rectangular blocks by using Taguchi method, considering angular displacement of the block with span and stream wise disposition. Kurtbas et al. (2009) experimentally examined the performances of heat transfer and friction loss in a round tube by constructing a novel conical twisted tape inserts. Al-Fahed et al. (1998) experimentally examined the behaviour of heat transfer and flow friction factor using oil as a functional fluid and then compared these results for a plain round tube, micro fins and tape inserts. Promvonge (2007b) carried out an experimental investigation to study the augmentation of thermal hydrodynamic performance of round tube fitted with numerous twisted tape shapes. In the experiment range of Reynolds number was varied from 3000 to 18000 laterally with three different pitch ratios ranging from 4.0 - 6.0. Chompoonokham et al. (2010) experimentally examine the behaviour of wedge obstacle and winglet vortex generators. It was discovered that the combined ribs and the WVG show the considerable enhancement in efficiency factor over the smooth passsage. Bartwal et al. (2018) experimentally investigated passive heat transfer enhancement technique. Air was used as a working fluid with the range of Reynolds number varied from 5000 to 40,000.

The maximum TEF of 2.84 is retrieved for the PR = 3, and G = 9. Akhavan-Behabadi et al. (2010) experimentally studied the augmentation of thermal hydraulic performance of round tube attached with various coiled wires inserts. Meng et al. (2005) examined the thermal hydraulic performance of round tube attached with vortex generator. Their analysis showed that the DDIR tube inserts have better thermal performance than the other tubes. Sarac and Bali (2007) experimentally studied the augmentation of thermal hydraulic performance of round tube attached with vortex generator. Their analysis showed that the decaying of the efficiency factor decreased steadily from the axial. Yang et al. (2011) investigated that the convergence of the tube can raise the stream rate which can decrease the turbulence generated in the stream and consequently there is decline in the heat transfer. Datt et al. (2018) presents the heat transfer and friction characteristics of turbulent circular tube flow through a square wing with combined solid ring twisted tape inserts which have been analyzed experimentally. The finest value of thermal and hydraulic performance has been found to be 2.74 for of 3,000 within the range of the parameters investigated.

Hong et al. (2019) investigated turbulent thermal and fluid flow characteristics of multiple twisted tapes (MTTs) inserted sinusoidal rib tube (SRT) heat exchangers. The results revealed that by inserting SRT there is increase in heat transfer enhancement of about 27.4%–39.5% and increased friction loss of around 49.4%–74.7% higher than that in the baseline of spirally corrugated tube (SCT), also the overall thermal performance was enhanced up to 1.59 for the alone use of SRT. Piriyarungrod et al. (2018) presents the thermo-hydraulic characteristics in the heat exchanger tube inserted with multiple-twisted tapes (M-TT). The experimental results found that the use of multiple-twisted tapes (M-TT) with N = 3, 4, 5 and 6 leads to the considerable increases in heat transfer enhancement and friction factor as compared to those of single twisted tape.

Farnam et al. (2018) explored that the heat transfer coefficient and pressure drop of the straight-tube and twisted-tube fitted with twisted-tapes are higher than those of the straight-tube and twisted-tube alone, and evidently, both the parameters increase with the decrease in the twist ratio. Eiamsa-ard, and Wongcharee (2018) developed Micro-fin tubes into which non-uniform twisted tapes were inserted in a counter-current arrangement gave higher heat transfer enhancement than the ones in a co-current arrangement. Karami et al. (2012) developed imperialist competitive algorithm is used to obtain optimize heat transfer rate in an air cooled heat exchanger fitted with the classic twisted tape inserts. According to the results, in order to obtain greatest heat transfer rate, the twist ratio must be at the lowest level.

Sarviya and Fuskele (2018) investigated heat transfer augmentation using a novel kind of twisted tape inserts with continuous cut edges. From obtained results it is evident that higher heat transfer rates can be achieved by employing twisted tape inserts with continuous cut edges at the cost of a reasonable pressure drop. Sarviya and Fuskele (2018) experimentally examined the thermal hydraulic performance of a heat exchanger tube equipped with various twisted tape widths and twist ratios. It can be seen that the combining effects of both the geometric and structural modifications, an improved design with optimum comprehensive performance was suggested.

Ayub et al. (2018) developed unique shell and tube heat exchanger with interstitial twisted tapes was tested with propylene glycol/water solution. From results it is clear new design heat exchanger showed better thermal enhancement index for the whole range of fluid concentrations. Lei et al. (2017) carried out numerical simulations to investigate the thermo-hydraulic performance of the two reformed shell-and-tube heat exchangers equipped with louver baffles. The numerical results revealed that the heat transfer coefficient per pressure drop of both the shell-and-tube heat exchangers with louver baffles are higher than that of the shell-and-tube heat exchanger with segmental baffles. Han et al. (2019) carried out multi-objective optimization of corrugated tube with loose-fit twisted tape to achieve the optimal performance, using response surface methodology and Non-dominated
Li et al. (2019) carried out a numerical investigation to conduct an air side heat transfer and pressure drop performance of twisted oval tube bundles with in line layout in cross flow. The results revealed that the twisted oval tube bundles perform excellent heat transfer performance compared with other tube bundles in cross flow. Li et al. (2019) the ratio of outer major axis to outer minor axis, twist pitch length, transverse tube pitch, longitudinal tube pitch and number of longitudinal tube rows on the air side heat transfer tube and pressure drop performance are examined, which reveals that the twisted oval tube is an aerodynamic tube that is free of the angle of attack. Tan et al. (2012) concluded that the emergence of twist in the twisted oval tube results in secondary flow and it is this secondary flow that enhances the total velocity and temperature distributions of the twisted oval tube. Saravanan and Jaisankar (2019) examined that the helix with V cut twisted tape insert has given better thermal performance than helix with square cut twisted tape insert for an identical twist ratio. Aroonrat and Wongwises (2019) determine the influence of dimpled depth on the condensation heat transfer coefficient and pressure drop of R-134a flowing inside circular dimpled tubes. Wang et al. (2019) investigated the heat transfer performance in laminar flow of a round tube equipped with a longitudinal vortex generator. Results reveal that multiple pairs of additional longitudinal vortexes are developed, and the fluid can rub the tube wall due to the concave shape surface of the insert.

Ponnada et al. (2019) effect of perforated twisted tapes with alternate axis, perforated twisted tapes and regular twisted tapes with different twist ratios are compared by experimental investigation in a circular tube under constant heat flux condition. At constant pumping power, the maximum thermal performance factor obtained is 1.433, 1.396 and 1.24 respectively for perforated twisted tapes with alternate axis, perforated twisted tapes and regular twisted tapes. Abolarin et al. (2019) experimentally investigate the heat transfer and pressure drop characteristics in a smooth circular tube with alternating clockwise and counter clockwise twisted tape inserts. An increase in heat flux significantly enhanced the heat transfer in the laminar flow regime and delayed transition. Geometries/parameters of various twisted tape inserts and correlations developed between the parameters by various investigators for heat transfer, pressure drop and thermal-hydraulic performance for different twisted tape inserts used in heat exchanger tubes are given in Table 1.

3. COMPARATIVE STUDY OF VARIOUS TWISTED TAPE INSERT HEAT EXCHANGER TUBES

From the investigation of heat transfer and pressure drop it is concluded that heat transfer in the twisted tape inserts in round tube is improved with a significant rise in the pressure drop. Thus, it is important to choose twisted tape geometry that should not only outperformed in heat transfer but also retain the pressure drop at a minimum possible level. In order to achieve this goal of simultaneous consideration of thermal as well as hydraulic performance a parameter that is taken in consideration is known as efficiency parameter. The optimum data selected for various parameters of the tape inserts are like, twist length, twist ratio, pitch ratio, twist angle, etc. Thermal hydraulic performance parameter of various twisted tapes has been determined using their corresponding correlations of heat transfer rate: friction factor and thermal hydraulic performance as listed in Table 1.

Figure 1 represents the multiple twisted tape inserts shape that provides the utmost value of thermal hydraulic performance with air as test fluid among all the twisted tape shapes examined. Figure 2 represents the multiple spiky twisted tape inserts shape that provides the utmost value of thermal hydraulic performance with water as test fluid among all the twisted tape shapes examined. Figure 3 represents the circular with center cleared twisted tape inserts shape provides the utmost value of thermal hydraulic performance with oil as test fluid among all the twisted tape shapes examined. In a dynamic air field stream, the roughness creates turbulence and improves the heat transfer/exchange by convection. The literature reveals that single twisted tape inserts in a tube of heat exchanger thermohydrodynamically performs best as compared to delta and helical twisted tape inserts, as the twist ratio induces multiple vortex stream cells which helps to enhancement of local heat transfer rate. Various investigators concluded that multi type twisted tape inserts in heated tube surface of a heat exchanger tube boost up the rate of heat transfer. Further it was concluded that the utilization of multiple twisted tape increases the number of vortex flow as compared to single twisted tape inserts, which helps to increase the heat transfer rate, as shown in Figure 4.
Fig. 2 Comparison of thermal hydraulic performance as function of Reynolds number for different type of twisted tape inserts with water as test fluid.

Fig. 3 Comparison of thermal hydraulic performance as function of Reynolds number for different type of twisted tape inserts with oil as test fluid.
Table 1 Correlations developed for heat transfer; pressure drop and thermal hydraulic performance in twisted tape insert heat exchanger tubes.

<table>
<thead>
<tr>
<th>Twisted tape geometry</th>
<th>Working fluid: Air</th>
<th>Parameters/optimum ranges</th>
<th>Correlations</th>
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<tbody>
<tr>
<td>Tube with solid rings and square wings TT inserts. Datt et al. (2018).</td>
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</table>
| Fluid: Air | Parameters: | | \[
N_{TT} = 0.0007R_e^{0.74}(d_d/D_T)^{0.17}B_o (d_R/D_T)^{0.17} \\
\times \left[1 - 0.18\ln\left(\frac{d_R}{D_T}\right)^2\right]\left(\frac{P_w}{W_T}\right)^{2.53} \\
\times \exp\left[-1.26\left(\frac{P_w}{W_T}\right)^2 \times \left(\frac{W_d}{W_T}\right)^{-0.78}ight] \\
\times \exp \left(-0.19\ln\left(\frac{W_T}{W_d}\right)\right)^2 \\
\times (d_R/d_{ctb})^{0.57} \exp\left(-2.3\left(\frac{d_R}{d_{ctb}}\right)^2 \times (N_{TT})^{0.69} \exp\left(-0.25\ln\left(N_{TT}\right)\right)^2 \right)
\] |
| Multiple squares perforated twisted tapes inserts. Singh et al. (2017). | | | |
| Fluid: Air | Parameters: | | \[
N_{TT} = 0.8306 H_{TT}^2 \left(\frac{d_{ctb}}{d_R}\right)^{1.485} \exp\left(-0.329\frac{\ln\left(H_{TT}T_{TT}\right)^2}{\ln\left(T_{TT}\right)^2}\right) \\
\times \exp\left(-0.136\ln\left(T_{TT}/T_{TT}\right)\right)^2 \\
f_{rs} = 2.68R_e^{0.4077}\left(\frac{a}{T_{TT}}\right) - 0.9735 \exp\left(-0.2978\ln\left(\frac{a}{T_{TT}}\right)^2\right) \\
\times \left(\frac{a}{T_{TT}}\right)^{1.841} \\
\times \exp\left(-1.2398\ln\left(T_{TT}/T_{TT}\right)\right)^2 \\
\eta_{p} = 0.44 \times 10^{-2} R_e^{0.62} H_{TT}^{1.7341} \exp\left(-0.625\frac{\ln\left(H_{TT}\right)^2}{\ln\left(T_{TT}\right)^2}\right) \\
\right)
\] |
| Solid ring with multiple twisted tapes inserts. Singh et al. (2016). | | | |
| Fluid: Air | Parameters: | | \[
N_{TT} = 0.09653 \left(Re_T^{0.7834}\right) N \times 0.0551 \exp(0.0256\ln N^2)T_R^{0.2127} \\
\times \exp\left(-0.1696\ln T_R^2\right)^2 \\
f_{rs} = 1.073 \left(R_e_T^{0.09766}\right) N \times 0.0352 \exp(0.1094\ln N^2)T_R^{0.4696} \\
\times \exp\left(-0.3766\ln T_R^2\right)^2 \\
\eta_{p} = 3.013 \left(R_e_T^{0.09766}\right) N \times 0.0180 \exp(0.1063\ln N^2)T_R^{0.1304} \\
\times \exp\left(-0.0968\ln T_R^2\right)^2 \\
N_{TT} = 0.0832 \left(R_e_T^{0.7899}\right) N \times 0.0393 \exp(0.0355\ln N^2)T_R^{0.23757} \\
\times \exp\left(-0.2488\ln T_R^2\right)^2 \\
f_{rs} = 1.042 \left(R_e_T^{0.0539}\right) N \times 0.0073 \exp(0.0772\ln N^2)T_R^{0.4780} \\
\times \exp\left(-0.3660\ln T_R^2\right)^2 \\
\eta_{p} = 2.94 \left(R_e_T^{0.0771}\right) N \times 0.0072 \exp(0.0237\ln N^2)T_R^{0.1097} \\
\times \exp\left(-0.0814\ln T_R^2\right)^2
\] |
| Fluid: Air | Parameters: | | \[
N_{TT} = 5.172 G_e^{0.3699} \left(Re_T\right)^{0.1411} \left(P_r_T^{0.2048} G^{1.434} \sin\theta^{0.33719}\right) \\
\times \frac{1}{\sqrt{\nu}} \\
f_{rs} = 17.355 \left(Re_T\right)^{0.94391} \left(sina\right)^{-0.18001} h_{c}^{-0.6215} t_{w}^{-0.67074} t_{tn}^{-0.375767} \\
\] |
| | | | |
| | | | |
| | | | |

Fluid: Air
Parameters:
5660 ≤ Re_\text{frs} ≤ 17000
Minimum and maximum values of results:
Nt_{\text{frs}} = 39 – 410
f_{\text{frs}} = 0.5 – 0.46.
η_\text{r} = 1.1 – 1.94.

Finally:
\[ Nt_{\text{frs}} = 0.185Re_{\text{frs}}^{-0.49}Pr_{\text{frs}}^{0.4} (y_{\text{fr}}/D_{\text{s}})^{-0.21} \]
\[ f_{\text{frs}} = 4.14Re_{\text{frs}}^{-0.25} (y_{\text{fr}}/D_{\text{s}})^{-0.21} \]
\[ Nt_{\text{frs}} = 2.29Re_{\text{frs}}^{0.49}Pr_{\text{frs}}^{0.4} (y_{\text{fr}}/D_{\text{s}})^{-0.21} \]
(TT taken in reverse directions for offset swirl)
\[ f_{\text{frs}} = 5.29Re_{\text{frs}} e^{-0.26} (y_{\text{fr}}/D_{\text{s}})^{-0.33} \]


Fluid: Air
Parameters:
72000 ≤ Re_{\text{frs}} ≤ 50,200
Minimum and maximum values of results:
Nt_{\text{frs}} = 80 – 290
f_{\text{frs}} = 0.032 0.14.
η_\text{r} = 1.3 – 1.6.

Finally:
\[ Nt_{\text{frs}} = 0.00023P_{\text{frs}} - 0.045Re_{\text{frs}}^{0.004} 0.065Re_{\text{frs}}^{0.004} + 0.075R_{\text{frs}}^{0.004} + 0.5601P_{\text{frs}}^{0.35} \]
\[ f_{\text{frs}} = 0.0073P_{\text{frs}} - 0.035Re_{\text{frs}}^{0.004} + 0.055Re_{\text{frs}}^{0.004} + 25.436Re_{\text{frs}} [0.0093P_{\text{frs}} - 0.022P_{\text{frs}} + 0.12P_{\text{frs}} - 0.6001] \]

Helical screw-tape. Kumar et al. (2013).

Fluid: Air
Parameters:
10 ≤ Re_{\text{frs}} ≤ 1000
Wire diameter 0.0769, 0.1026
Helix angle 30°, 60°
Minimum and maximum values of results:
Nt_{\text{frs}} = 5 – 132
f_{\text{frs}} = 0.02 – 1.2.
η_\text{r} = 1.45 – 1.71.

Finally:
\[ N_t_{\text{frs}} = 5.172 \left[ l + \exp \left[ 0.908 \sin^2 \theta \right] \left( d/D_{\text{s}} \right)^{0.6493} \right] \]
\[ f_{\text{frs}} = 17.355 \left( \frac{\sin \theta}{\sqrt{d/D_{\text{s}}}} \right)^2 \]
\[ (1 + 10^{-9}Sw^{2.67})^{1/7} \times [1 + \exp(0.05538. \sin \theta)/(d/D_{\text{s}})]^{0.0902} \times [1 + \exp(0.07685)] \]


Fluid: Air
Parameters:
4021 ≤ Re_{\text{frs}} ≤ 16116
y_\text{frs} = 1.75, 2.3, 2.9 and 3.5
Minimum and maximum values of results:
Nt_{\text{frs}} = 49.07 – 116.19

Finally:
\[ Nt_{\text{frs}} = 0.96P_{\text{frs}}^{0.18} \left( \frac{P_{\text{frs}}}{D_{\text{s}}} \right)^{-0.18} \]
\[ Nt_{\text{frs}} = 0.053Re_{\text{frs}}^{0.706}P_{\text{frs}}^{0.4} \left( \frac{y_{\text{frs}}}{W} \right)^{-0.127} \left( \frac{y_{\text{frs}}}{W} \right)^{-0.388} \]
\[ f_{\text{frs}} = 12053Re_{\text{frs}}^{-0.2959} \left( \frac{y_{\text{frs}}}{W} \right)^{-0.652} \left( \frac{y_{\text{frs}}}{W} \right)^{-1.513} \]


Fluid: Air
Parameters:
2000 ≤ Re_{\text{frs}} ≤ 6000
2y_\text{frs} = 2.0, 2.50, 3.10
Pitch ratios 1.5 & 3.0
Minimum and maximum values of results:
Nt_{\text{frs}} = 35 – 120
f_{\text{frs}} = 0.03 – 0.042.
η_\text{r} = 1.29.

Finally:
\[ Nt_{\text{frs}} = 0.101Re_{\text{frs}}^{1.73}Pr_{\text{frs}}^{0.4} (e_p)^{-0.265} (e_w)^{-0.287} \]
\[ f_{\text{frs}} = 0.89Re_{\text{frs}}^{0.994}Pr_{\text{frs}}^{0.4} (e_p)^{-0.516} (e_w)^{-0.656} \]
(T-W towards the back wing set up)
\[ Nt_{\text{frs}} = 0.11Re_{\text{frs}}^{0.731}Pr_{\text{frs}}^{0.4} (e_p)^{-0.283} (e_w)^{-0.316} \]
\[ f_{\text{frs}} = 0.55Re_{\text{frs}}^{-0.138} (e_p)^{-0.683} (e_w)^{0.759} \]
(T-W towards the back wing set up)


Fluid: Air
Parameters:
830 ≤ Re_{\text{frs}} ≤ 1990
y_\text{frs} = 3.0
Density of nanofluid varied from 0.30% to 0.70%.
Minimum and maximum values of results:
Nt_{\text{frs}} = 12 – 67
f_{\text{frs}} = 0.32 – 0.67.
η_\text{r} = 1.5 – 5.4.

Finally:
\[ Nt_{\text{frs}} = 0.026Re_{\text{frs}}^{0.927} (Pr_{\text{frs}})^{0.4} (\phi_{\text{frs}} + 1)^{0.128} (\text{Tube with TT with alternative axis}) \]
\[ Nt_{\text{frs}} = 0.005Re_{\text{frs}}^{0.406} (Pr_{\text{frs}})^{0.4} (\phi_{\text{frs}} + 1)^{0.112} (\text{TTT}) \]
\[ f_{\text{frs}} = 3.23Re_{\text{frs}}^{-0.308} (\phi_{\text{frs}} + 1)^{0.082} \]
\[ Nt_{\text{frs}} = 0.027Re_{\text{frs}}^{0.693} (\phi_{\text{frs}} + 1)^{0.094} \]
\[ Nt_{\text{frs}} = 0.006Re_{\text{frs}}^{0.832} (\phi_{\text{frs}} + 1)^{0.0850} \]
Multiple typical twisted tapes. Sarada et al. (2010).

Fluid: Air
Parameters:
$6000 \leq Re_\infty \leq 13500$
Widths of the TT 10.0mm to 22.0 mm.

Minimum and maximum values of results:
$N_{u_\infty} = 30 - 45$
$f_{rs} = 0.0072 - 0.0079.$
$\eta_{rs} = 1.1 - 1.7.$


Fluid: Air
Parameters:
$3700 \leq Re_\infty \leq 21000$
Pitch ratios 2.5, 3.5 and 4.0
Perforated holes $N = 4, 6$ and 8.

Minimum and maximum values of results:
$N_{u_\infty} = 27 - 188$
$f_{rs} = 0.031 - 0.052.$
$\eta_{rs} = 1.4.$


Fluid: Air
Parameters:
$3000 \leq Re_\infty \leq 27000$
$y_d = 3.0, 4.0,$ and 5.0

Minimum and maximum values of results:
$N_{u_\infty} = 43 - 265$
$f_{rs} = 0.03 - 0.052.$
$\eta_{rs} = 1.34.$

Periodically varying wire coil. Elamsa-ard et al. (2010).

Fluid: Air
Parameters:
$4600 \leq Re_\infty \leq 20000$
Two various $y_d = 3.0, 4.0$ of TT of varying three coils pitch ratios.

Minimum and maximum values of
$N_{u_\infty} = 15 - 148$
$f_{rs} = 0.032 - 0.053.$
$\eta_{rs} = 1.1 - 1.25.$


Fluid: Air
Parameters:
$3000 \leq Re_\infty \leq 27000$
$y_d = 3.0, 4.0$ and 5.0.

Minimum and maximum values of
$N_{u_\infty} = 27 - 274$
$f_{rs} = 0.05 - 0.31.$
$\eta_{rs} = 1.05 - 1.95.$


Fluid: Air
Parameters:
$4000 \leq Re_\infty \leq 19000$
$y_d = 3.0, 4.0,$ and 5.0.

Minimum and maximum values of results:
$N_{u_\infty} = 16 - 72$
$f_{rs} = 0.03 - 0.15.$
$\eta_{rs} = 0.8 - 1.2.$

Fluid: Air
Parameters:
$4000 \leq Re_\infty \leq 20000$
Tape length ratios are $0.29, 0.43, 0.57$ and 1.0.

$$N_{u_\infty} = 0.414 \times 10^{0.0556(Re_\infty)^{0.001(H/w)}^{0.001(D_b/L)^{-0.141}}}.$$  

$$f_{rs} = 0.0139 Re_\infty^{-0.1374} [0.001 + Re_\infty]^{-0.001} (D_b/L)^{-0.2097}.$$  

$$N_{u_\infty} = 0.473 Re_\infty^{-0.666} Pr_{rs}^{-0.4} (y_d/w)^{-0.053}$$  

$$f_{rs} = 72.29 Re_\infty^{-0.966} Pr_{rs}^{-0.4} (y_d/w)^{1.01}$$  

$$N_{u_\infty} = 0.264 Re_\infty^{-0.666} Pr_{rs}^{-0.4} (y_d/w)^{-0.61}$$  

$$f_{rs} = 41.7 Re_\infty^{-0.525} (y_d/w)^{-0.846}$$  

$$N_{u_\infty} = 1.84 Re_\infty^{-0.086} (y_d/w)^{-0.038}$$

$$N_{u_\infty} = 0.31 Re_\infty^{-0.6} Pr_{rs}^{-0.4} (y_d/w)^{-0.36} (1 + \sin \theta)^{-0.44}$$  

$$f_{rs} = 46.39 Re_\infty^{-0.544} (y_d/w)^{-0.77} (1 + \sin \theta)^{-0.45}$$  

$$N_{u_\infty} = 2.93 Re_\infty^{-0.043} (y_d/w)^{-0.77} (1 + \sin \theta)^{-0.31}$$

$$N_{u_\infty} = 0.197 Re_\infty^{-0.708} Pr_{rs}^{-0.4} (1 + S)^{-0.244}$$  

$$f_{rs} = 12.133 Re_\infty^{-0.232} Pr_{rs}^{-0.0362}$$  

$$N_{u_\infty} = 0.186 Re_\infty^{-0.713} Pr_{rs}^{-0.4} (1 + S)^{-0.249}$$  

$$f_{rs} = 22.366 Re_\infty^{-0.277} Pr_{rs}^{-0.449}$$

$$N_{u_\infty} = 0.182 Re_\infty^{-0.67} Pr_{rs}^{-0.4} (y_d/w)^{-0.224} (1 + d/w)^{0.082}$$  

$$f_{rs} = 21.7 Re_\infty^{-0.045} Pr_{rs}^{-0.04} (y_d/w)^{-0.564} (1 + d/w)^{0.676}$$  

$$N_{u_\infty} = 2.346 Re_\infty^{-0.0435} Pr_{rs}^{-0.6} (y_d/w)^{-0.0304} (1 + d/w)^{0.356}$$

$$N_{u_\infty} = 0.06 Re_\infty^{0.75} Pr_{rs}^{-0.4} (y_d/w)^{-0.26}$$  

$$f_{rs} = 10.02 Re_\infty^{-0.65} Pr_{rs}^{-0.0564} (y_d/w)^{-0.36}$$  

$$N_{u_\infty} = 0.069 Re_\infty^{0.74} Pr_{rs}^{-0.4} (y_d/w)^{-0.26} [1.5(s/D_d) + 1]^{-0.1}$$  

$$f_{rs} = 30.5 Re_\infty^{-0.56} (y_d/w)^{-0.256} [1.5(s/D_d) + 1]^{-0.2}$$  

$$N_{u_\infty} = 0.066 Re_\infty^{0.693} Pr_{rs}^{-0.4} L_{RS}^{-0.122}$$  

$$f_{rs} = 2.8 Re_\infty^{-0.0366} L_{RS}^{-0.19}$$
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<tr>
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</thead>
<tbody>
<tr>
<td>Short-length twisted tape inserts.</td>
<td>Minimum and maximum values of $N_{U_{rs}} = 12 - 58$</td>
<td>Minimum and maximum values of $N_{U_{rs}} = 12 - 174$</td>
<td>$N_{U_{rs}} = 52 - 125$</td>
<td>Minimum and maximum values of $N_{U_{rs}} = 50 - 350$</td>
<td>$N_{U_{rs}} = 62 - 280$</td>
<td>Minimum and maximum values of $N_{U_{rs}} = 10 - 87$</td>
<td>$N_{U_{rs}} = 10 - 90$</td>
</tr>
<tr>
<td></td>
<td>$f_{rs} = 0.03 - 0.05$, $\eta_{s} = 0.9 - 1.17$.</td>
<td>$f_{rs} = 0.5 - 3.0$, $\eta_{s} = 0.5 - 1.57$.</td>
<td>$f_{rs} = 0.5 - 0.9$, $\eta_{s} = 1.3 - 1.7$.</td>
<td>$f_{rs} = 0.12 - 0.25$, $\eta_{s} = 0.98 - 1.28$.</td>
<td>$f_{rs} = 0.3 - 0.48$, $\eta_{s} = 0.9 - 1.4$.</td>
<td>$f_{rs} = 0.1 - 0.24$.</td>
<td>$f_{rs} = 0.05 - 0.24$, $\eta_{s} = 1.2 - 1.76$.</td>
</tr>
<tr>
<td>Fluid: Air, Parameters:</td>
<td>$3000 \leq Re_{rs} \leq 18000$, Pitch ratios of 4.0, 6.0 and 8.0, $y_{rs} = 4.0, 6.0$.</td>
<td>Fluid: Air, Parameters: $11543 \leq Re_{rs} \leq 108166$, $y_{rs} = 2.0, 4.4$.</td>
<td>Fluid: Air, Parameters: $6.0, 8.0$. $y_{rs} = 2.0, 1.5, 2.5, y = 1, 1.5, 2, and y = 2.5$.</td>
<td>Fluid: Air, Parameters: $1000 \leq Re_{rs} \leq 40000$, $y_{rs} = 2.0, 1.5, 2.0, y_{rs} = 1, 2, 2.5$.</td>
<td>Fluid: Air, Parameters: $5000 \leq Re_{rs} \leq 25000$, $y_{rs} = 1.56, 1.87, 2.82$.</td>
<td>Fluid: Air, Parameters: $5000 \leq Re_{rs} \leq 15000$, $y_{rs} = 6.0, 8.0$ and space ratio of 1.0, 2.0, 3.0.</td>
<td>Fluid: Air, Parameters: $5000 \leq Re_{rs} \leq 20000$, $y_{rs} = 6.0, 8.0$. Space ratios are 1.0, 2.0, 3.0.</td>
</tr>
<tr>
<td></td>
<td>$N_{U_{rs}} = 12 - 58$, $f_{rs} = 0.03 - 0.05$, $\eta_{s} = 0.9 - 1.17$.</td>
<td>Minimum and maximum values of results: $N_{U_{rs}} = 12 - 174$</td>
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<td>Minimum and maximum values of results: $N_{U_{rs}} = 10 - 90$</td>
</tr>
<tr>
<td></td>
<td>$f_{rs} = 338.37Re_{rs}^{-0.367}CR^{-0.887}Y_{rs}^{-0.4660}$ and $0.5(Pr_{rs}^{0.4})CRe^{-0.382}Y_{rs}^{-0.38}$</td>
<td></td>
<td>$N_{U_{rs}} = 0.23(Term1 + Term2)(1/AR + 0.1)^{0.15} \frac{(\varepsilon/D_{rs})^{0.0541}}{(\varepsilon/e)^{0.192}}$</td>
<td></td>
<td>$N_{U_{rs}} = (0.364 + 3.66e^{-1.11y})Re_{rs}^{0.08 - 0.375e^{-0.33y}}Pr_{rs}^{1/3}$</td>
<td>$N_{U_{rs}} = 0.144Re_{rs}^{-0.697}Pr_{rs}^{0.4}(s + 1) - 0.179$</td>
<td>$N_{U_{rs}} = 0.0101Re_{rs}^{0.929}(1 + S)^{-0.266}$</td>
</tr>
<tr>
<td></td>
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<td></td>
<td>$N_{U_{rs}} = 0.023(Term1 + Term2)(1/AR + 0.1)^{0.15} \frac{(\varepsilon/D_{rs})^{0.0541}}{(\varepsilon/e)^{0.192}}$</td>
<td>$f_{rs} = 0.12 - 0.25$, $\eta_{s} = 0.98 - 1.28$.</td>
<td>$f_{rs} = 0.3 - 0.48$, $\eta_{s} = 0.9 - 1.4$.</td>
<td>$f_{rs} = 0.1 - 0.24$.</td>
<td>$f_{rs} = 0.05 - 0.24$, $\eta_{s} = 1.2 - 1.76$.</td>
</tr>
</tbody>
</table>

Fluid: Air, Parameters: $1000 \leq Re_{rs} \leq 40000$, $y_{rs} = 2.0, 1.5, 2.0, y_{rs} = 1, 2, 2.5$. Minimum and maximum values of results: $N_{U_{rs}} = 12 - 174$.

$f_{rs} = 0.5 - 3.0$, $\eta_{s} = 0.5 - 1.57$. Minimum and maximum values of results: $N_{U_{rs}} = 12 - 174$.

$N_{U_{rs}} = 52 - 125$.

$N_{U_{rs}} = 0.023(Term1 + Term2)(1/AR + 0.1)^{0.15} \frac{(\varepsilon/D_{rs})^{0.0541}}{(\varepsilon/e)^{0.192}}$ (Regular spaced TT)

Fluid: Air  
Parameters:  
200 ≤ \(Re_{rs}\) ≤ 11000  
Angular vane angle \(\theta_{rs}\) = 15°, 30°, 45°, 60° and 75°.  
Minimum and maximum values of results:  
\(Nu_{rs} = 67 - 392\)  
\(f_{rs} = 3.5 - 16.8\)  
\(η_p = 1.67\).

### Square duct with twisted tape inserts. Ray and Date (2001).

Fluid: Air  
Parameters:  
30 ≤ \(Re_{rs}\) ≤ 1100  
\(y_{rs}\) = 1.5 to 10, \(Pr_{rs}\) = 0.1 to 500.  
Minimum and maximum values of results:  
\(Nu_{rs} = 5 - 120\)  
\(f_{rs} = 0.3 - 1.2\).


Fluid: Air  
Parameters:  
110 ≤ \(Re_{rs}\) ≤ 1500  
\(y_{rs}\) = 1.63 to 5.28.  
\(G_{rs}\) = 8.1-82.0.  
Minimum and maximum values of results:  
\(Nu_{rs} = 3.0 - 10\).

### Twisted tape geometry

<table>
<thead>
<tr>
<th>Working fluid</th>
<th>Parameters/optimum ranges</th>
<th>Correlations</th>
</tr>
</thead>
<tbody>
<tr>
<td>Water</td>
<td></td>
<td></td>
</tr>
<tr>
<td>SRT-4 twisted tapes insert. Hong et al. (2019).</td>
<td></td>
<td></td>
</tr>
<tr>
<td>Fluid: Water</td>
<td></td>
<td></td>
</tr>
<tr>
<td>Parameters:</td>
<td></td>
<td></td>
</tr>
<tr>
<td>(5000 ≤ Re_{rs} ≤ 10000)</td>
<td>(y/w=2.5, 5, 10, 15, 20 and 25)</td>
<td></td>
</tr>
</tbody>
</table>
| Rib pitch to diameter ratios at 0.27–1.53, rib height to diameter ratios at 0.02–0.056 and corrugation angles at 9.2°–37.0° | \(Nu_{rs} = 27.4\%–39.5\%\) | \(f_{rs} = 2.66–10.07\)  
\(η_p = 1.59\) and 1.49. |

### Multiple twisted tapes. Piriyarungrod et al. (2018).

Fluid: Water  
Parameters:  
\(6000 ≤ Re_{rs} ≤ 20000\)  
\(y/w=2.5, 5, 10, 15, 20\) and 25  
\(Nu_{rs} = 1.13, 1.18, \text{ and } 1.2\)  
\(f_{rs} = 0.14–0.20\)  
\(η_p = 1.2\).

### Typical twisted tape inserts. Maddah et al. (2014).

Fluid: Water/ Nanofluid  
Parameters:  
\(5000 ≤ Re_{rs} ≤ 21000\)  
\(y_{rs}\) = 1.03 to 4.  
Minimum and maximum values of results:  
\(Nu_{rs} = 50 - 210\)  
\(f_{rs} = 0.04 - 0.075\)  
\(η_p = 1.3 - 1.89\).
### Schematic diagram of Classic twisted tape. Karami et al. (2012).

**Fluid**: Water, Parameters: 11.00 ≤ 𝑑 ≤ 16,116
(y/w = 1.76 to 3.53)

\[ \frac{Nu_{rs}}{\beta} = 147.827 \]

\[ \eta_{\beta} = 1.76 \]

### Geometries of twisted tapes. Murugesan et al. (2012).

**Fluid**: Water, Parameters: 2000 ≤ 𝑑 < 12000

\[ \frac{Nu_{rs}}{\beta} = 2.0 \]

Minimum and maximum values of results:

\[ Nu_{rs} = 18 - 130 \]

\[ f_{rs} = 0.03 - 0.29 \]

\[ \eta_{\beta} = 1.05 - 1.5 \]

### Tubes equipped with twin twisted tapes. Zhang et al. (2012).

**Fluid**: Water, Parameters:

\[ \frac{Nu_{rs}}{\beta} = 8.2 - 13.5 \]

\[ f_{rs} = 0.2 - 1.3 \]

\[ \eta_{\beta} = 1.6 - 2.3 \]


**Fluid**: Water, Parameters:

\[ \frac{Nu_{rs}}{\beta} = 4.0 - 23 \]

\[ f_{rs} = 0.03 - 0.09 \]

\[ \eta_{\beta} = 1.21 - 1.41 \]


**Fluid**: Water, Parameters:

\[ \frac{Nu_{rs}}{\beta} = 11 - 64 \]

\[ f_{rs} = 0.25 - 0.62 \]

\[ \eta_{\beta} = 2.2 - 5.4 \]


**Fluid**: Water, Parameters:

\[ \frac{Nu_{rs}}{\beta} = 6.11 \]

\[ f_{rs} = 0.04 - 0.18 \]

### V-cut Twisted tapes inserts. Murugesan et al. (2011).

**Fluid**: Water, Parameters:

\[ \frac{Nu_{rs}}{\beta} = 0.0296 \]

\[ f_{rs} = 0.08 - 0.29 \]

\[ \eta_{\beta} = 1.02 - 1.29 \]

---

\[ Nu_{rs} = 90.2 + 14.7Re - 3.72Re - 0.276Re^2 - 0.539Re \times R \]

\[ f_{rs} = 2.642Re^{0.474}Y^{0.392} \]

\[ Nu_{rs} = 0.0276e^{0.8629}Pr_{rs}^{0.33}Y_{rs}^{-0.215} \text{ and} \]

\[ f_{rs} = 10.7564Re_{rs}^{0.387}Y_{rs}^{-1.054} \]

\[ Nu_{rs} = 0.128Re_{rs}^{0.723}Pr_{rs}^{0.64}(e_{p})^{-0.188}(e_{w})^{0.318} \text{ and} \]

\[ f_{rs} = 1.1439Re_{rs}^{0.723}Pr_{rs}^{0.64}(e_{p})^{-0.198}(e_{w})^{0.339} \]

\[ Nu_{rs} = 2.0358Re_{rs}^{0.238}(\alpha)^{0.0497}(TTT), \text{ and} \]

\[ f_{rs} = 1.1439Re_{rs}^{0.723}Pr_{rs}^{0.64}(e_{p})^{-0.198}(e_{w})^{0.339} \]

\[ Nu_{rs} = 0.783Re_{rs}^{0.44}Pr_{rs}^{0.59}(Y_{rs})^{3.65}(1 + S/D_{rs})^{-0.124}\text{ and} \]

\[ f_{rs} = 121.69Re_{rs}^{0.904}Y_{rs}^{-0.055}(1 + S/D_{rs})^{-0.0515} \text{ (For phase 1)} \]

\[ Nu_{rs} = 0.0017Re_{rs}^{0.906}Pr_{rs}^{0.5437}Y_{rs}^{-0.5437} \text{ and} \]

\[ f_{rs} = 0.907 \text{ (TTT)} \]

\[ Nu_{rs} = 6.11Re_{rs}^{0.199}(1 + x)^{-0.664}Y_{rs}^{-0.3118} \text{ and} \]

\[ f_{rs} = 54.41Re_{rs}^{0.87}(1 + x)^{-0.945}Y_{rs}^{-0.146} \]

\[ Nu_{rs} = 0.0296Re_{rs}^{0.0853}Pr_{rs}^{0.33}Y_{rs}^{-0.222}(1 + |d_{max}/w|)^{1.148}(1 + |w/W|)^{-0.715} \text{ or tubes fitted with v-twist TT} \]

\[ f_{rs} = 8.632Re_{rs}^{-0.0615}Y_{rs}^{-0.269}(1 + |d_{max}/w|^{2.477})(1 + |w/W|)^{-1.914} \]

---
Peripherally-cut and alternate axis twisted tape. Seemawute et al. (2010).

Fluid: Water
Parameters: 5000 ≤ \(Re_{TS}\) ≤ 20000
Peripherally-cut TT with alternate axis 1.25, 1.11 and 1.02.
Minimum and maximum values of
\(N_{u_{TS}} = 45 - 275\)
\(f_{r_{TS}} = 0.12 - 0.5\)
\(\eta_p = 1.05 - 1.25\).

Right-left helical twist with ratio 4.89
Right-left helical twist ratio 3.91
TT with left-right helical screw.
Nagarajan et al. (2010).

Fluid: Water, Parameters: 5000 ≤ \(Re_{TS}\) ≤ 15000
Stream ratio 0.004 to 0.01
Minimum and maximum values of results:
\(N_{u_{TS}} = 40 - 510\)
\(f_{r_{TS}} = 0.5 - 1.6\)
\(\eta_p = 1.2 - 4.1\).

Dimple tube with twisted tape inserts. Thianpong et al. (2009).
Fluid: Water
Parameters: 12000 ≤ \(Re_{TS}\) ≤ 44000
\(y_r = 3.0, 5.0, \text{and} 7.0\)
Minimum and maximum values of results:
\(N_{u_{TS}} = 55 - 457\)
\(f_{r_{TS}} = 0.06 - 0.24\)

Twisted tape inserts. Sharma et al. (2009).
Fluid: Water
Parameters: 3500 ≤ \(Re_{TS}\) ≤ 8500
0 ≤ \(H/D\) ≤ 15,
4.5 ≤ \(Pr\) ≤ 5.5
Minimum and maximum values of results:
\(N_{u_{TS}} = 30 - 90\)
\(f_{r_{TS}} = 0.04 - 0.09\)
\(\eta_p = 1.2 - 1.4\).

Fluid: Water
Parameters: 12000 ≤ \(Re_{TS}\) ≤ 44000
\(y_r = 3.0, 5.0, \text{and} 7.0\)
Minimum and maximum values of results:
\(N_{u_{TS}} = 20 - 160\)
\(f_{r_{TS}} = 0.01 - 0.13\)
\(\eta_p = 0.9 - 1.48\).


\[ Nu_{TS} = 0.422Re_{TS}^{0.544}Pr_{TS}^{0.4} \left(\frac{W}{W}\right)^{-0.148} \]
\[ f_{r_{TS}} = 59.08Re_{TS}^{0.615} \left(\frac{W}{W}\right)^{-0.18} \]

\[ Nu_{TS} = 0.3962(y)^{-0.3866}Pr_{TS}^{0.3}(Re_{TS})^{0.6717}(Pr_{TS})^{0.4} \]
\[ f_{r_{TS}} = 2.811(y)^{-0.3966}Pr_{TS}^{0.63}(Re_{TS})^{0.478}(Pr_{TS})^{0.44}(Pr_{TW})^{0.14} \]
\[ f_{r_{TS}} = 739.2(y)^{-0.634}(Re_{TS})^{1.013}(Pr_{TS})^{-0.2} \]

\[ Nu_{TS} = (0.323 + 0.1366 \times e^{-1164xAW}) \times Re_{TS}^{0.79} - 0.135xe^{-1074xAW} \]

\[ Nu_{TS} = 3.138 \times 10^{-3}(Re_{TS})(Pr_{TS})^{0.66}(1.0 + H_{TS}/D_{TS})^{0.02}(\phi + 1)^{1.22} \]
\[ f_{TS} = 173(Re_{TS})^{-0.06}(1.0 + H_{TS}/D_{TS})^{2.15}(\phi + 1)^{2.15} \]
\[ (\text{For} \ \phi_r = 10.16, Re_{TS} < 7000, \ \text{Clockwise twist}) \]

\[ Nu_{TS} = 0.1949Re_{TS}^{0.71415} \]
\[ Nu_{TS} = 0.02564Re_{TS}^{0.9724} \]
\[ f_{TS} = 8.029Re_{TS}^{0.6367}f_{r_{TS}} = 0.021Re_{TS}^{0.60} \]
\[ f_{TS} = 0.061Re_{TS}^{0.1015} \]

\[ Nu_{TS} = 0.258Re_{TS}^{0.554}(Pr_{TS})(Pr_{TS})^{-0.42} (1 + s/D_{TS})^{-0.042} \]
\[ f_{TS} = Re_{TS}^{-0.384} \]
\[ f_{TS} = 0.852(1 + s/D_{TS})^{-0.047} \]

H}
Twisted tape inserts with conical-ring. Promvonge et al. (2007).

Fluid: Water
Parameters: 6000 \( \leq R_e_{rs} \leq 26000 \)
\( \eta_{rs} = 3.75 \) and 7.5.
Minimum and maximum values of results:
\( N_U_{rs} = 125 \) to 223
\( f_{rs} = 4 \) to 6.1.
\( \eta_{rs} = 1.2 \) to 1.9.

Horizontal pipe with helical ribs. Naphon et al. (2006).

Fluid: Water
Parameters: 15000 \( \leq R_e_{rs} \leq 60000 \)
\( \eta_{rs} = 3.1 \) to 5.5.
Minimum and maximum values of results:
\( N_U_{rs} = 40 \) to 110
\( f_{rs} = 1 \) to 1.6.
\( \alpha = 2.5 \) to 6.6.


Fluid: Water
Parameters: 2700 \( \leq R_e_{rs} \leq 13500 \)
\( \eta_{rs} = 1.95 \), 2.93, 3.91 and 4.89.
Minimum and maximum values of results:
\( N_U_{rs} = 11 \) to 80
\( f_{rs} = 0.1 \) to 0.6.

Helical screw tape. Iivashanmugam et al. (2006).

Fluid: Water
Parameters: 200 \( \leq R_e_{rs} \leq 3000 \)
Minimum and maximum values of results:
\( N_U_{rs} = 10 \) to 70
\( f_{rs} = 0.1 \) to 0.55.
\( \eta_{rs} = 1.3 \) to 1.82.

Regularly spaced twisted tape inserts. Saha et al. (2004).

Fluid: Oil
Parameters: Rib Pitch: 2.0437, 5.6481, Rib Height = 0.07692, 0.1026.
Centre clearance = 0, 0.2, 0.4, 0.6
Minimum and maximum values of results:
\( N_U_{rs} = 6 \) to 150.5
\( f_{rs} = 0.5 \) to 1.0 . \( \eta_{rs} =1.0\) to 1.32.

Twisted tape geometry
Working fluid: Oil
Parameters/optimum ranges
Correlations

Circular with center-cleared twisted tapes. Saha et al. (2012).

Fluid: Oil
Parameters: Rib Pitch: 2.0437, 5.6481, Rib Height = 0.07692, 0.1026.
Centre clearance = 0, 0.2, 0.4, 0.6
Minimum and maximum values of results:
\( N_U_{rs} = 0.022 \) to 1.2
\( f_{rs} = 30 \) to 165.
\( \eta_{rs} = 1.2 \) to 1.48.

\[ N_{U_{rs}} = 1.365R_e_{rs}^{0.433}P_{rs}^{0.40}(d_{rs}/D_{rs})^{-1.230}\eta_{rs}^{-0.0530} \quad \text{and} \]
\[ f_{rs} = 24.870R_e_{rs}^{-0.430}(d_{rs}/D_{rs})^{-3.990}\eta_{rs}^{-0.160} \]

\[ N_{U_{rs}} = 0.648R_e_{rs}^{0.36}(P_{rs})^{1/3}\eta_{rs}^{-0.0533} f_{rs} \geq 3 \]
\[ f_{rs} = 3.517R_e_{rs}^{-0.414}(P_{rs})^{1/3}\eta_{rs}^{-0.0533} f_{rs} \geq 3 \]

\[ N_{U_{rs}} = 0.467R_e_{rs}^{0.4774}(P_{rs})^{1/3}\eta_{rs}^{-0.0533} f_{rs} \geq 3 \]
\[ f_{rs} = 32.415R_e_{rs}^{-0.598}(P_{rs})^{1/3}\eta_{rs}^{-0.0533} f_{rs} \geq 3 \]

\[ N_{U_{rs}} = 0.725(R_e_{rs}^{0.568}y_{rs}^{-0.708}(P_{rs})^{1/3}(\mu_b/\mu_w)^{0.14}(\text{heating}) \]
\[ f_{rs} = 3.165R_e_{rs}^{0.517}(y_{rs}^{-1.05}(P_{rs})^{1/3}(\mu_b/\mu_w)^{0.14}(\text{cooling}) \]

\[ N_{U_{rs}} = 5.172 \left( \frac{1 + (29/\pi)^{0.1346}(y_{rs}^{0.0584})}{(P_{rs})^{0.1346}} \right)^{2.18} \times \frac{1.6538 \times 10^{-15}(R_e_{rs}R_f)^{2.18}}{1 + (29/\pi)^{0.1346}(y_{rs}^{0.0584})} \times B, \]
\[ f_{rs} = 45.812\left[ 1 + 10^{-6}(R_e_{rs}y_{rs}^{-1.05})^{2.07} \right]^{2.18} \times (AR)^{-1.39} \times [1 + (29/\pi)^{0.1346}(y_{rs}^{0.0584})] \times A. \]

Fluid: Oil
Parameters: \( \gamma_{rs} = 2.5 \) and \( Pr_{rs} = 320 - 545 \). Centre clearance = 0, 0.2, 0.4, 0.6
Minimum and maximum values of results: \( Nu_{rs} = 5 - 148 \), \( \eta_p = 0.9 - 1.18 \).

\[
N_{u_{rs}} = 5.172 \left[ 1 + 0.89322G_x^{0.9125} + 1.82273 \times 10^{-6}a_{sw, Pr_{rs}^{0.667}} \right]^{2.9} \\
+ 1.5638 \times 10^{-15} \left( Re_{rs} Ra_{3} \right)^{2.15} \\
\left( \frac{\mu_{rs}}{\mu_{sw}} \right)^{0.14} \left( \frac{1}{AR} + 0.1 \right)^{0.15} + \left( \frac{e}{D} \right)^{0.0740 \times 0.195} \\
(1 + 10^{-6} Sw^{2.67})^{1/7} \\
(AR)^{1.47} \times \left( 1 + \frac{e}{(D/e)^{0.883}} \right) \\
\text{(Short length TT with internal rib)}
\]


Fig. 4 Fluid flow pattern (A) single tape insert (B) double tape insert (C) multiple tape insert
4. CONCLUSIONS

This article presents a critical review of work done in the area of hydrodynamic and thermal performance using twisted tapes. The effect of various twisted tape inserts parameters on hydrodynamic and thermal performance are discussed in detail. The following conclusions can be drawn:

1. The applications of twisted tape inserts in a heat exchanger tube are an efficient method to enhance the heat transfer to fluid flow in the round heat exchanger tube. The reduction of the twist pitch values and tube diameter ratio tends to increase the heat transfer rate and pressure drop as well.

2. The twist angle is the most significant structural factor. A higher twist angle leads to larger hydrodynamic and thermal performance. More the twist angle, the higher tangential velocity will be created. As the twist angle increases, the hydrodynamic and thermal performance decreases slowly.

3. Reducing values of the twist pitch to tube diameter ratio, lead to increased values of heat transfer rate and pressure drop as well. Swirl flow helps in decreasing the boundary layer thickness of the hot air flowing and rises the residence time of hot air in the inner tube.

4. Augmentation of thermal performance in full length twisted tape is better than the twist fitted with rod and spacer. The decrease in heat transfer augmentation in twisted fitted with rod is minimum compared to twist fitted with rod is minimum compared to twist fitted with spacer. The decrease in pressure drop is better for twist fitted with spacer compared to twist fitted with rod.

5. V-cut twisted tape offered a higher local Nusselt number, local friction factor and also thermal hydraulic performance as compared to plain twisted tape. In addition, the influence of the depth ratio was more dominant than that of the width ratio for all the flow parameters.

6. Using any kind of twisted tape leads to thermal hydraulic improvement which is more substantial for lower values of excess air flow rate. Comparison of heat transfer performance shows that the improvement of convection heat transfer coefficient is more than total heat transfer coefficient.

7. Among the entire twisted tape elements examined, the multiple twisted tape inserts have the maximum value of hydrodynamic and thermal performance than that of other twisted tape shapes for the examined range of twisted tape parameters.

NOMENCLATURE

- \( D_{rs} \): Diameter of Tube [m]
- \( d_{rs} \): Director diameter [m]
- \( P_{rs} \): Wetted perimeter [m]
- \( e_{rs} \): Diameter of wire [m]
- \( h_{rs} \): Heat transfer coefficient (W/m²K)
- \( S_{rs} \): Swirl parameter (m)
- \( q_{rs} \): Heat flux (W/m²)
- \( G_{rs} \): Graetz number
- \( f_{rs} \): Friction factor
- \( P_{rs} / H_{rs} \): Rib pitch ratio
- \( P_{rs} \): Prandtl number
- \( g \): Acceleration due to gravity
- \( CFD \): Computational fluid dynamics
- \( HET \): Heat exchanger tube
- \( TT \): Twisted tape
- \( TTT \): Typical Twisted tape
- \( WVG \): Winglet type vortex generators
- \( PCR \): Perforated conical ring

REFERENCES


